#### **Virial Expansion**

#### Silicon Valley FIG

March 24, 2018

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#### **Virial Expansion**

#### This paper was uploaded to Wikipedia.

# Google 'virial expansion' and you will find it.

Let's first scan through it on Wiki.



#### Summary

- <u>Second and Third Virial</u> <u>Coefficients</u>
- <u>Casting Equations of State into</u> <u>Virial Form</u>
- Cubic Virial Equation of State
- Gas-Liquid-Solid Equilibrium
- State of Virial Equations



## Gas-Liquid-Solid Equilibrium

Since 1972, I have struggled with the possibility of describing gas-liquid-solid equilibrium with an equation of state.

I picked up this problem again in 2015. After several try-and-error attempts, now I have a very simple virial equation of state doing exactly that.





#### The ideal gas law: Pv = RT

#### It can be states in terms of compressibility: Z=Pv/RT=1



## **Virial Equation of State**

Virial equation of state for real gases: Z=Pv/RT =A+B/v+C/v<sup>2</sup>+D/v<sup>3</sup>+E/v<sup>4</sup>+F/v<sup>5</sup>+ ...

A=1: real gases behave like ideal gas when v is large.





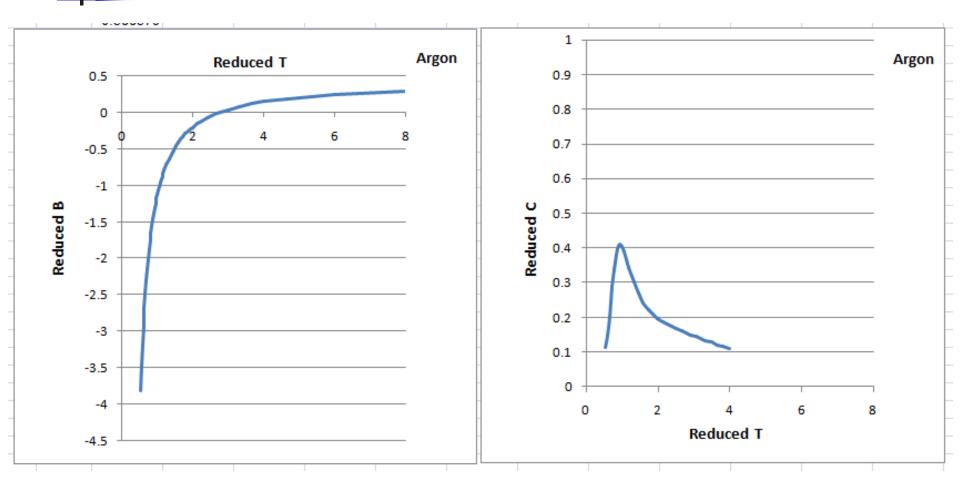
#### **B: Second virial coefficient represents bimolecular attraction.**

**C:** Third virial coefficient represents tri-molecular repulsion.

etc...



#### 2nd and 3rd Virial Coefficients



## **3<sup>rd</sup> Virial Coefficent**

My expectation is that the third virial coefficient must be a monotonically decreasing function of temperature. Otherwise, liquid could not coexist with gas below the critical temperature.

Accurate equations of state should confirm my expectation.



#### **Some Equations of State**

Van der Waals EOS (1873)  $P=RT/(V-b)+a/V^2$ Kamerlingh Onnes EOS (1901)  $P=(RT/V)(1+B/V+C/V^2+D/V^4+E/V^6+F/V^8)$ Benedict-Webb-Rubin EOS (1940) Starling EOS (1972)  $P=RT/V+B/V^2+C/V^3+D/V^6$  $+(E/V^3)(1+F/V^2)exp(-F/V^2)$ 



#### **Cast EOS into Virial Forms**

#### **Van der Waals EOS** P=RT/(V-b)+a/V<sup>2</sup>

**Cast it into virial equation of state:**  $P=(RT/V)(1+(b-a/RT)/V+b^2/V^2+b^3/V^3+...)$ 

Third virial coefficient is a constant, and obviously not correct.



#### **Cast EOS into Virial Forms**

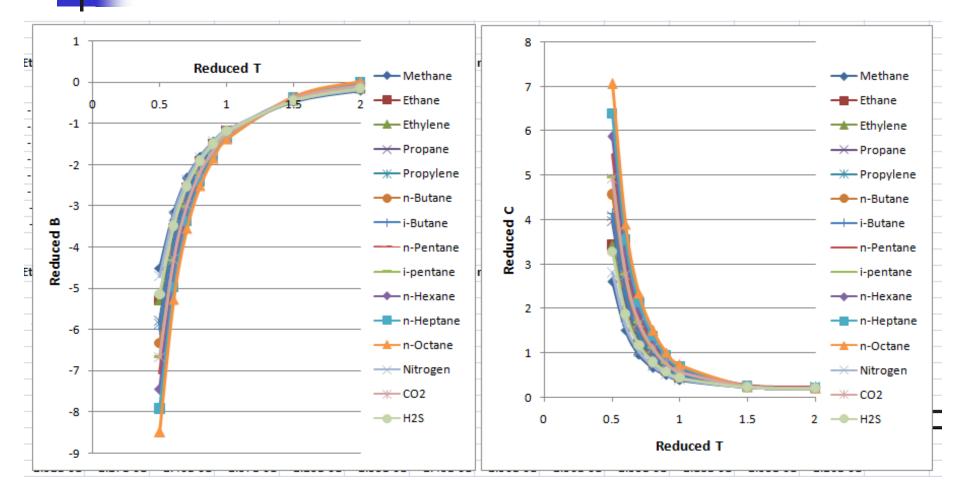
#### Benedict-Webb-Rubin EOS $P=RT/V(1+(B_0-A_0/RT-C_0/RT^3)/V+(b-a/RT)/V^2 + aa/RTV^4+(c/RT^3V^2)(1+\gamma/V^2)exp(-\gamma/V^2))$

Cast it into virial equation of state:  $P=RT/V(1+(B_0-A_0/RT-C_0/RT^3)/V + (b-a/RT+c/RT^3)/V^2 + aa/RTV^4 + (c\gamma/RT^3V^6))$ 

Third virial coefficient is a monotonically decreasing function of T.



#### 2<sup>nd</sup> and 3<sup>rd</sup> Virial coefficients from Starling



## **Cubic Virial Equation**

Benedict-Webb-Rubin and Starling EOS can be reduced to: P=RT/v+B/v<sup>2</sup>+C/v<sup>3</sup>+F/v<sup>5</sup>

If F/v<sup>5</sup> is ignored, we have a cubic virial equation of state: P=RT/v+B/v<sup>2</sup>+C/v<sup>3</sup>



## **Cubic Virial Equation**

The cubic virial equation has all the nice properties of van der Waals equation of state, without the singularity at v=b.  $Z=(RT/v)(1+B/v+C/v^2)$ 

At critical temperature: B=- $v_c$ , C= $v_c^2/3$  and Z<sub>c</sub>= $P_cv_c/RT_c=1/3$ 



## **Gas-Liquid Equilibrium**

#### Gas and liquid phases are in equilibrium under saturation pressure: $P_{sat}=RT_{sat}(1+B/v+C/v^2)/v$

It can be rearranged as:  $1-(RT_{sat}/P_{sat})(1+B/v+C/v^2)/v = 0$ 



#### **Gas-Liquid Equilibrium**

In the saturation region, the cubic equation has three roots, and can be written alternatively as:  $(1-v_l/v)(1-v_m/v)(1-v_g/v)=0$ 

which can be expanded as:  $1-(v_1+v_g+v_m)/v+(v_1v_g+v_gv_m+v_mv_l)/v^2-v_1v_gv_m/v^3=0$ 



#### **Gas-Liquid Equilibrium**

From these two identical equations:  $1-(RT_{sat}/P_{sat})(1+B/v+C/v^2)/v=0$   $1-(v_l+v_g+v_m)/v+(v_lv_g+v_gv_m+v_mv_l)/v^2$  $-v_lv_gv_m/v^3=0$ 

 $v_m$ , B, C and can be solved:  $v_m = RT_{sat}/P_{sat}-v_l-v_g$   $B=-(v_lv_g+v_gv_m+v_mv_l)/(RT_{sat}/P_{sat})$  $C=v_lv_gv_m/(RT_{sat}/P_{sat})$ 



## **Cubic Virial Equation**

#### The cubic virial equation: Z=(RT/v)(1+B/v+C/v<sup>2</sup>)

- More accurate than van der Waals EOS.
- No singularity.
- Compatible with Benedict-Webb-Rubin and Starling EOS.
- Virial coefficients can be derived from PVT data and from saturation properties.



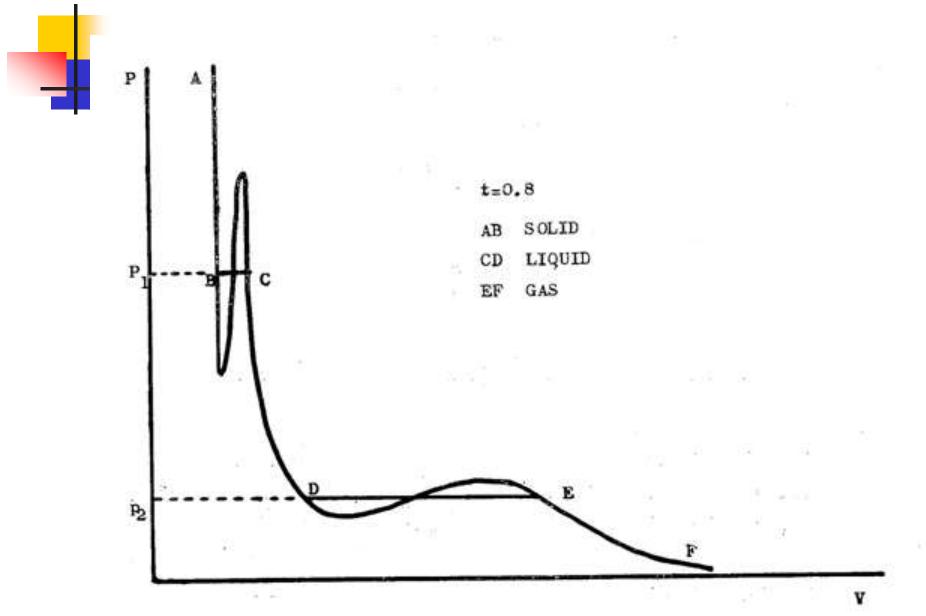
## Gas-Liquid-Solid Equilibrium

Cubic virial EOS can be extended for gasliquid-solid equilibrium: P=(RT/V)(1+B/V+C/V<sup>2</sup>+U/V<sup>n</sup>+W/V<sup>2n</sup>)

U/V<sup>n</sup> depresses PVT isotherm, and W/V<sup>2n</sup> pushes the isotherm up to form an Sshaped bend between  $v_s$  and  $v_l$ . The bend must be very sharp and very steep, requiring very high power factor n.



#### **Gas-Liquid-Solid Equilibrium**



## **Properties of Argon**

| Property   | Value   | Reduced Value |
|--|---------|---------------|
| Critical Point Volume (dm <sup>3</sup> /mole)  | 0.07459 | 1             |
| <b>Critical Point Temperature (°K)</b>   | 150.687 | 1             |
| <b>Critical Point Pressure (MPa)</b>   | 4.863   | 1             |
| Critical Compressibility (Z <sub>c</sub> =P <sub>c</sub> V <sub>c</sub> /RT <sub>c</sub> ) | 0.291   | 0.291         |
| Triple Point Vapor Volume (dm <sup>3</sup> /mole)  | 9.853   | 132.1         |
| Triple Point Liquid Volume (dm <sup>3</sup> /mole)   | 0.0282  | 0.378         |
| Triple Point Solid Volume (dm <sup>3</sup> /mole)  | 0.0246  | 0.330         |
| Triple Point Temperature (°K)  | 83.8058 | 0.553         |
| <b>Triple Point Pressure (MPa)</b>   | 0.06889 | 0.0142        |



## Gas-Liquid-Solid Equilibrium in Argon

The best virial EOS is with n=30:  $p=(t/vZ_c)(1-b/v+c/v^2-(v_u/v)^n+(v_w/v)^{2n})$ 

For Argon at the triple point t=0.553, p=0.0142,  $Z_c=0.291$   $v_s=0.330$ ,  $v_l=0.378$ 

b=3.424, c=1.152 n=30 , v<sub>u</sub>=0.3443 , v<sub>w</sub>=0.335



## Gas-Liquid-Solid Equilibrium in Argon

# The best virial EOS is with n=30. The isotherm is plotted with three separated terms:

$$p_1 = (t/vZ_c)(1+b/v+c/v^2)$$
  

$$p_2 = (t/vZ_c)(v_u/v)^n$$
  

$$p_3 = (t/vZ_c)(v_w/v)^{2n}$$
  

$$p = p_1 - p_2 + p_3$$



#### **Gas-Liquid-Solid Equilibrium of Argon** 5 4 3 2 1 p1 p p2 0 0.35 • p2 03 0.4 0.45 0.5 v -1 р -2 -3 -4 -5





#### The best virial EOS is with n=30:

$$P = (t/vZ_c)(1-3.424/v+1.152/v^2) - (0.3443/v)^{30} + (0.3350/v)^{60}$$



#### **Virial Coefficients**

#### Virial EOS for gas-liquid-solid equilibrium: P=(RT/V)(1+B/V+C/V<sup>2</sup>+U/V<sup>n</sup>+W/V<sup>2n</sup>)

- B represents bimolecular attraction.
- C represents tri-molecular repulsion.
- U represents molecular attraction in liquid phase.
- W represents repulsion among molecules locked in crystal lattice.



#### **Virial Coefficients**

## n-2n potential well with n=30 seems excessive.

In liquid phase, an argon atom has 12 nearest neighbors, and up to 32 next nearest neighbors.

In solid phase, interacting neighbors are infinite in a crystal lattice.



#### Conclusions

- 3<sup>rd</sup> Virial coefficient is a monotonically decreasing function of T.
  - A cubic virial EOS  $P=RT/v+B/v^2+C/v^3$

accurately prescribes gas-liquid equilibrium.

The cubic virial EOS can be extended P=(RT/V)(1+B/V+C/V<sup>2</sup>+U/V<sup>n</sup>+W/V<sup>2n</sup>) for gas-liquid-solid equilibrium.

## **State of Virial Equations**

- For every fluid, its cubic virial EOS has to be solved before considering high virial terms.
- Virial EOS can be solved with Excel. Multi-variable optimization is not necessary, and its results are not to be trusted.
- For the first time in history, gas-liquidsolid equilibrium is quantitatively represented by a virial equation of state.





#### **Thank You Very Much!**

